

# Structural Effects on the High Temperature Adsorption of CO<sub>2</sub> on a Synthetic Hydrotalcite

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Hydrotalcite-like compounds (HTlcs) are solid sorbents that may potentially be used for high-temperature separation and capture of CO<sub>2</sub>. The high-temperature adsorption of CO<sub>2</sub> on Mg–Al–CO<sub>3</sub> HTlc is affected by structural changes that take place upon heating of the material. The structural changes of a synthetic HTlc upon heating to 200 and 400 °C in a vacuum were characterized using various analytical techniques. These structural changes were then related to observed behavior with respect to the physisorption and chemisorption of CO<sub>2</sub> at 200 °C. Upon heating to 200 °C, the material retains its layered structure, though the interlayer spacing is decreased by ~0.6 Å due to loss of interlayer water. Chemisorption of CO<sub>2</sub> at 200 °C represents more than half of the total adsorption capacity (at 107 kPa) due to increased availability of the framework Mg<sup>2+</sup> cation and the subsequent formation of MgCO<sub>3</sub>. There is no significant increase of surface area or pore volume after heating to 200 °C. Upon heating to 400 °C the CO<sub>3</sub><sup>2-</sup> in the interlayer is decomposed and the material is completely dehydrated and partially dehydroxylated. The resulting amorphous 3-D structure with increased surface area and pore volume and decreased availability of the Mg<sup>2+</sup> cation favors physisorption over chemisorption for these samples. An increased understanding of structure–property relationships will help in the further development of HTlcs as viable CO<sub>2</sub> solid sorbents.

## Introduction

Increases in the atmospheric concentrations of gases such as methane (CH<sub>4</sub>), nitrous oxide (N<sub>2</sub>O), and, especially, carbon dioxide (CO<sub>2</sub>) have enhanced the heat-trapping capability of the earth's atmosphere via the greenhouse effect. There are known ways to manage the emission of greenhouse gases. Increases in the efficiency of energy use are largely responsible for reduction of U.S. greenhouse gas intensity (the amount of greenhouse gases emitted in relation to economic growth) in the past 10 years. Carbon emissions may also be reduced by increasing the use of carbon-free or low-carbon energy sources (e.g., nuclear, biomass, solar, wind). A relatively new concept for the control of carbon emissions is that of carbon sequestration. In this option, carbon dioxide is captured and securely stored for long-term sequestration.

The costs of separation and capture, including compression, are estimated to make up about three-fourths of the total costs of ocean or geologic sequestration.<sup>1</sup> Currently, the most likely options for CO<sub>2</sub> separation

and capture are (1) chemical and physical absorption, (2) physical and chemical adsorption, (3) low-temperature distillation, (4) gas separation using membranes, and (5) mineralization. Among these, physical absorption using amine solvents is the only technology that is currently deployed commercially for CO<sub>2</sub> capture. However, there is a significant energy penalty associated with this technology from the heat required to regenerate the solvent (though some recent improvements have lessened this penalty). The goals of the carbon sequestration program are for technologies that result in <10% increase in the cost of energy for direct capture/sequestration and <\$10 per metric ton of CO<sub>2</sub> that is indirectly sequestered.<sup>2</sup>

Selective adsorption has been identified as one of the ways to prevent the emission of CO<sub>2</sub> from fossil-fueled power plants and other sources. Pressure, vacuum, and temperature swing adsorption (PSA, VSA, and TSA, respectively) are proven technologies that are commonly used for many gas separations<sup>3</sup> and have been proposed for CO<sub>2</sub> separation and capture.<sup>4–8</sup> In the PSA opera-

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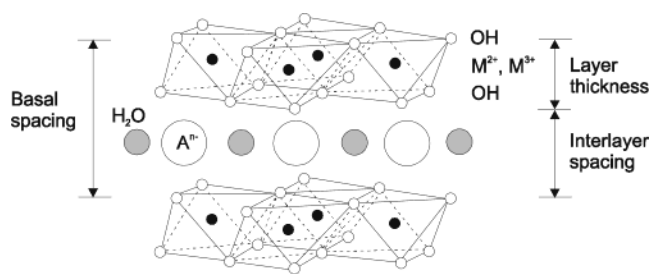
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tion, gases are selectively adsorbed at high pressure, isolated, and then desorbed by reducing the pressure. VSA is a simple variant of PSA, with a vacuum desorption cycle. In the TSA operation, the gases are adsorbed at lower temperature and desorbed by heating the sorbent bed. Recently, new adsorption cycles have been proposed. In these novel systems, enriching reflux and dual reflux PSA cycles are used in lieu of the traditional stripping reflux cycles that severely limit the enrichment of the heavy component.<sup>9,10</sup>

Many naturally occurring and synthetic materials have a high adsorption capacity for CO<sub>2</sub>. An International Energy Agency (IEA) study evaluated CO<sub>2</sub> separation and capture using both PSA and TSA operational modes and employing 13X zeolite as the sorbent. The IEA report<sup>11</sup> concluded that PSA and TSA technologies are not economically attractive for the gas- and coal-fired power systems included in that study. This conclusion has led many to extrapolate the findings and to conclude that adsorption systems are not applicable for CO<sub>2</sub> separation and capture. This, however, is not necessarily true. It is true that the most commonly studied adsorbents (zeolites and activated carbons) suffer from low capacity at elevated temperatures and are thus limited to operation at lower temperatures. It is also true that the viability of an adsorptive separation process is clearly linked to the applicability of the sorbent. It follows then that, in order for adsorption technologies to be effective and viable for separation and capture of CO<sub>2</sub>, new sorbents must be developed and tested. New sorbents are needed that have (1) high selectivity and adsorption capacity for CO<sub>2</sub> at elevated temperatures, (2) adequate adsorption/desorption kinetics for CO<sub>2</sub> at operating temperatures, (3) stable CO<sub>2</sub> capacity after repeated adsorption/desorption cycles, and (4) good hydrothermal and mechanical stability.<sup>12</sup>

Hydrotalcite-like compounds (HTLcs), also known as layered double hydroxides (LDHs) and anionic clays are bidimensional basic solids that have been used as catalysts, as adsorbents and ion exchangers for treatment of liquid wastes, and also in medicine (as antacids). The structure consists of positively charged brucite (magnesium hydroxide)-like layers with interlayer space containing charge compensating anions and water molecules.<sup>13</sup> The metal cations occupy the centers of octahedra whose vertexes contain hydroxide ions. The octahedra are connected by edge sharing to form an infinite sheet.<sup>14</sup> The general formula of the compounds is  $[M^{2+}_{1-x}M^{3+}_x(OH)_2]A^{n-}_{xm}$ , where M<sup>2+</sup> and M<sup>3+</sup> are



**Figure 1.** Structure of hydrotalcite-like compounds.

divalent (Mg<sup>2+</sup>, Zn<sup>2+</sup>, Ni<sup>2+</sup>, etc.), and trivalent cations (Al<sup>3+</sup>, Cr<sup>3+</sup>, etc.), A<sup>n-</sup> is a nonframework charge-compensating anion (such as CO<sub>3</sub><sup>2-</sup>, Cl<sup>-</sup>, SO<sub>4</sub><sup>2-</sup>), and *x* is normally between 0.17 and 0.33.<sup>13</sup> The structure is shown in Figure 1.

Published results of CO<sub>2</sub> sorption on hydrotalcite-like compounds (HTLcs) suggest that sorbents in this family may be useful for CO<sub>2</sub> separation and capture using adsorption technologies at high temperatures.<sup>12,15–18</sup> The most interesting result (reported by Yong et al.<sup>18</sup>) is that the CO<sub>2</sub> adsorption capacity follows the trend  $Q_{300} > Q_{20} > Q_{200}$  (where  $Q_T$  is the adsorption capacity at 1 atm and temperature *T*, °C). The authors suggested that this is due to a decrease of the interlayer (*d*) spacing between room temperature and 200 °C, resulting in less void space, which inhibits CO<sub>2</sub> adsorption. The authors further suggested that, at 300 °C, dehydroxylation and decarbonation of the HTlc results in structural modifications and increased porosity and an enhanced adsorption capacity for CO<sub>2</sub>. Others have shown that promotion by alkali salts can increase both the adsorption capacity and the stability of hydrotalcite-like adsorbents.<sup>16,17,19</sup> Other enhancements have been described, such as small additions of rare earth elements to the hydrotalcite structure.<sup>20</sup> There have been numerous studies that have described the thermal decomposition of hydrotalcite and other LDHs.<sup>21–23</sup> In this work we have attempted to describe and quantify the decomposition and structural modifications of an HTlc in N<sub>2</sub>, CO<sub>2</sub>, and mixed N<sub>2</sub>/CO<sub>2</sub> and to determine how those structural modifications affect the CO<sub>2</sub> adsorptive capacity of the HTlc.

## Experimental Section

**Synthesis of Hydrotalcite.** The HTlc used in this work was synthesized using a coprecipitation technique. The sample was prepared as a synthetic analogue of the naturally occurring hydrotalcite mineral,  $[Mg_{0.75}Al_{0.25}(OH)_2](CO_3)_{0.125} \cdot mH_2O$ .

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In the synthesis procedure, 0.75 mol of Mg(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O and 0.25 mol of Al(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O were dissolved in 250 mL of deionized (DI) water. The resulting solution was then added, drop-by-drop with vigorous stirring, to a 500 mL solution containing 1.7 mol of NaOH and 0.5 mol of Na<sub>2</sub>CO<sub>3</sub>. The resulting precipitate was then separated by vacuum filtration, washed with DI water, and dried at 100 °C in a conventional oven. The dried solid was then crushed in a mortar and pestle and stored in a glass sample bottle for subsequent characterization.

**Chemical Analysis.** Chemical analysis was done using X-ray fluorescence (XRF) on pellets prepared by mixing 2 g of the analyte with 2 mL (200 mg dry solids) of liquid binder to give a 32 mm diameter pellet weighing 2.2 g with a material-to-diluent ratio of 0.1. The XRF intensities were collected on each side of the pellet using Phillips SuperQ data collection software and evaluated using Omega Data System's UniQuant 4 XRF "standardless" data analysis software. The UQ/UQ calibration was used to analyze the samples. The pellets were evaluated as oxides.

**Surface Area and Porosity.** The surface area (BET), meso- and microstructure, and pore size distribution (PSD) of the HTLcs were calculated from N<sub>2</sub> adsorption isotherms at -196 °C that were obtained using a static volumetric system (Quantachrome Autosorb-1-C). The isotherms were measured using samples that had been pretreated by heating in a vacuum at various temperatures for a minimum of 12 h. (Note: all of the samples had originally been dried at 100 °C in air). The surface area was calculated using the BET method; the mesopore volume and diameter were calculated using the density functional theory (DFT) methodology.<sup>24</sup> Micropore volume and diameter (width) were calculated using the Horvath-Kawazoe (H-K) equation.<sup>24,25</sup>

**Thermal Treatment.** Differential scanning calorimetry (DSC) scans were obtained using a Perkin-Elmer DS7. Thermogravimetric analysis (TGA) was done using a Perkin-Elmer TG7. Thermal decomposition products were measured using a Pfeiffer Vacuum Prisma mass spectrometer during in situ heating of the sample under flowing helium in the chemisorption cell of a Quantachrome Autosorb-1C-MS.

**X-ray Diffraction.** High-temperature X-ray diffraction (HTXRD) patterns were collected at the High-Temperature Materials Laboratory at the Oak Ridge National Laboratory. X-ray diffraction (XRD) data were collected with a PANalytical X'Pert Pro theta-theta diffractometer using Cu K $\alpha$  X-radiation. The sample stage was an Anton Paar XRK900 reactor chamber. The powder sample was packed into a macor glass-ceramic sample holder that was spun during data collection to improve the counting statistics. Two thermocouples were used to control the heating elements to provide minimal temperature gradients in the heating volume. Incident optics consisted of a 0.25° divergence slit, 0.04 rad axial divergence Soller slits, and a 0.5° antiscatter slit; receiving optics consisted of a 5 mm antiscatter slit, 0.04 rad axial divergence Soller slits, and a Ni Cu K $\beta$  filter.

The detector was an X'Celerator real time multiple strip detector that collected data over a ~2.1° range simultaneously. All XRD data were collected with a step size of 0.0167° 2 $\theta$  and a scan rate of 0.133° 2 $\theta$ /s. Using the X'Celerator detector, high-quality diffraction patterns with excellent signal-to-background were collected in 4–10 min per scan.

In situ diffraction data were collected over a temperature range of 25–600 °C in flowing gases of CO<sub>2</sub>, N<sub>2</sub>, and a N<sub>2</sub>/CO<sub>2</sub> (80/20 vol %) mixture. The gas mixture was obtained using mass flow controllers set to 80 mL N<sub>2</sub>/min and 20 mL CO<sub>2</sub>/min. The system was flushed with gas for several minutes before beginning the in situ XRD scans. The XRD patterns were collected from 5° to 80° 2 $\theta$ ; each pattern took less than 10 min to collect. XRD patterns were collected at 25 °C and then from 100 to 200 °C in 25 °C steps, from 200 to 300 °C in

steps of 10 °C for the CO<sub>2</sub> and 80/20 mixture gases or 20 °C for the N<sub>2</sub> gas, from 300 to 400 °C in 10 °C steps, and finally from 400 to 600 °C in 50 °C steps. The heating rate was 20 °C/min.

**CO<sub>2</sub> Adsorption Isotherm Measurements.** High-temperature CO<sub>2</sub> adsorption isotherms were measured using the chemisorption cell of the Quantachrome Autosorb-1C-MS. The combined (physisorption plus chemisorption) isotherm was measured first. The sample was then evacuated, removing only the physically (weakly) adsorbed gas, and the adsorption isotherm measurement was repeated to obtain the physisorption component. The chemisorption (strong) isotherm was then determined by the difference in the combined isotherm and the physisorption (weak) isotherm. Additions of the adsorbate gas were made at volumes required to achieve a targeted set of pressures. A minimum equilibrium interval of 20 min with a tolerance of 0.5% for  $P > 1$  Torr and 1.7% for  $P < 1$  Torr was used to determine equilibrium for each measured point (i.e., the equilibrium criteria was checked every 20 min).

## Results

**Chemical Analysis.** The composition of the sample was determined to be [Mg<sub>0.73</sub>Al<sub>0.27</sub>(OH)<sub>2</sub>](CO<sub>3</sub>)<sub>0.135</sub>·*m*H<sub>2</sub>O (very close to the target). The hydrotalcite structure was then confirmed by X-ray diffraction. The average weight loss after heating to 120 °C was 7.9% (assumed to be the loss of loosely held water).

**Surface Area and Porosity.** The adsorption capacity of an adsorbent often follows the total surface area, since there are usually more available active binding/sorption sites on a material with higher surface area. The surface and porosity of the materials after various heat pretreatments were calculated from a variety of methods using data from the adsorption of N<sub>2</sub> at -196 °C (i.e. in a liquid N<sub>2</sub> bath). The N<sub>2</sub> at -196 °C adsorption isotherms for the HTLc after heating to 200 and 300 °C are shown in Figure 2. Both isotherms have a similar aspect and correspond to type IV according to the IUPAC 1985 classification of physisorption isotherms. The type IV isotherm, whose initial region is closely related to the type II isotherm, tends to level off at high relative pressures.<sup>26</sup> Both isotherms exhibit hysteresis, which is usually associated with the filling and emptying of the mesopores by capillary condensation. The hysteresis loop for the isotherm is of the type H3, which is affected by phenomena such as delayed pore condensation, percolation, and pore blocking and also by what is known as the tensile strength effect.<sup>27,28</sup> The volume adsorbed was much higher for the material after dehydration at 300 °C in vacuo, indicating a higher total surface area. The adsorption isotherms for materials dehydrated at 120 and 400 °C were very similar to those that had been dehydrated at 200 and 300 °C respectively (but are not shown for simplicity). The results for the calculated values of BET surface area and meso- and microporosity are given in Table 1. One can see that there is a significant increase in the surface area for the material after being preheated in a vacuum to 300 and 400 °C (177.4 and 183.7 m<sup>2</sup>/g, respectively) over the same material that was heated in a vacuum to 120 and 200 °C (55.3 and 66.1 m<sup>2</sup>/g, respectively).

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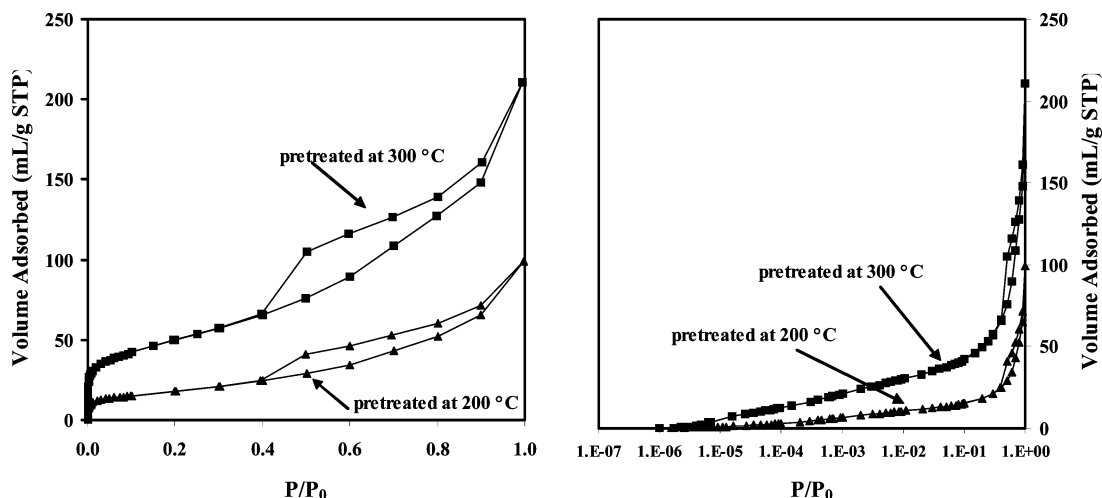
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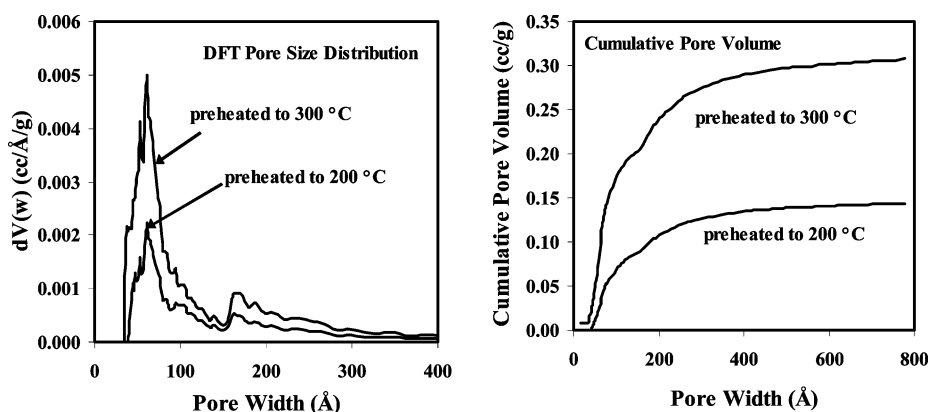
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**Figure 2.** Adsorption of  $N_2$  at  $-196$  °C on hydrotalcite after thermal pretreatment at  $200$  °C (lower curve) and  $300$  °C (upper curve). The isotherms are shown on a log scale on the right to better present the low-pressure region.



**Figure 3.** Mesopore size distribution (left) and cumulative mesopore volume (right) for hydrotalcite after thermal pretreatment at  $200$  °C (lower curve) and  $300$  °C (upper curve). The mesopore structures were calculated from  $N_2$  at  $-196$  °C adsorption isotherm data using the DFT method.

**Table 1. Surface Area and Porosity of HTlc Derived from  $N_2$  Adsorption at  $-196$  °C after Thermal Pretreatment at the Specified Temperatures**

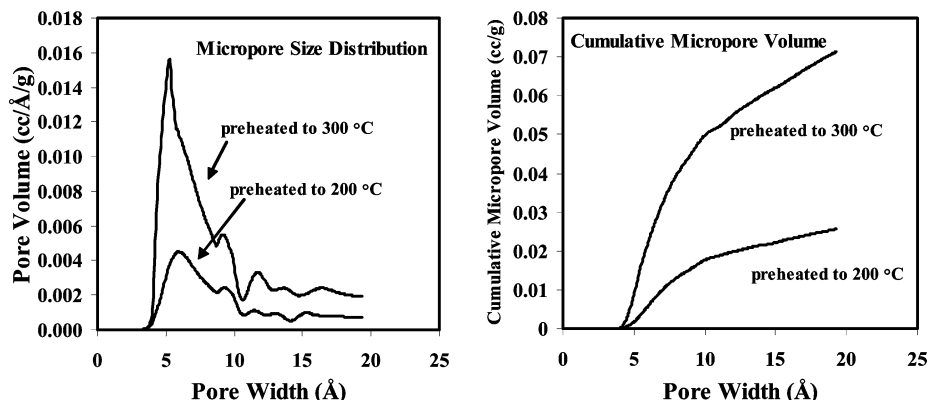
pretreatment temp, <sup>a</sup> °C	BET SA, m <sup>2</sup> /g	DFT <sup>b</sup>		HK <sup>c</sup>	
		$\Sigma V_p$ , cm <sup>3</sup> /g	$D_p$ , Å	$\mu D_p$ , Å	$\mu V_p$ , cm <sup>3</sup> /g
120	55.3	0.136	60.79	6.33	0.021
200	66.1	0.144	60.79	5.93	0.026
300	177.4	0.308	60.79	5.28	0.071
400	183.7	0.305	60.79	5.13	0.073

<sup>a</sup> Temperature at which the sample was heated prior to analysis; all samples were heated at the indicated temperature, in vacuo, for a minimum of 12 h. <sup>b</sup> Density functional theory <sup>c</sup> Horvath–Kawazoe equation assuming slit-type pores

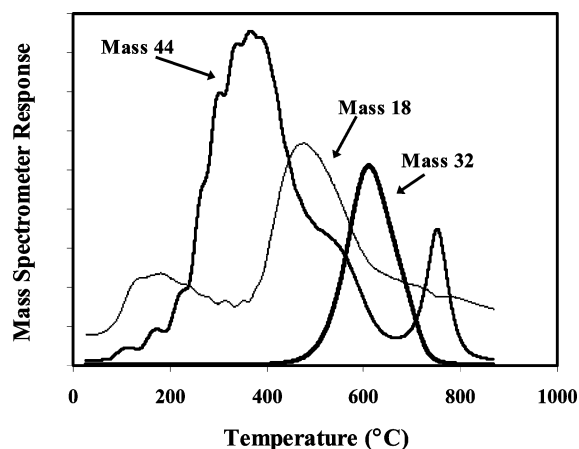
**Mesoporosity (Pores in the Range 20–500 Å).** The mesoporosity was evaluated using the DFT method. The mesopore size distribution and cumulative mesopore volume are shown in Figure 3. The results of the analysis are given in Table 1. There is an increase in the cumulative total pore volume (as calculated by the DFT method) with increasing pretreatment temperature with a large increase between the material that had been heated to 200 and 300 °C. However, the mesopore size distribution does not change with increasing pretreatment temperature; all of the materials were calculated to have a peak pore width of approximately 61 Å.

**Microporosity (Pores < 20 Å).** The microporosity was evaluated using the H–K equation with slit-type pores. The micropore size distribution and cumulative micropore volume are shown in Figure 4. The results of the analysis are given in Table 1. There is an increase in the cumulative micropore volume (as calculated using the H–K equation) with increasing pretreatment temperature and, as with the mesopore volume, there is a large increase for the materials that had been heated to 300 and 400 °C. However, unlike that of the mesopore size distribution, there is a change in the peak micropore width with increasing pretreatment temperature. The material has a peak micropore size of approximately 6.33 Å after heating to 120 °C. The peak micropore size decreases more than 1 Å to approximately 5.13 Å after heating to 400 °C. The micropore size distribution, given in Figure 4, shows the peak in the 5–6.5 Å range and a second smaller peak in the 8–10 Å range (consistent with the D–R plot prediction of multiple types of micropores).

**Thermal Decomposition.** To understand the structural effects on  $CO_2$  adsorption, it is important to understand the dehydration and decarbonation of the material. This was done in a series of experiments. First, the decomposition products were measured by heating the material from room temperature to 900 °C in a chemisorption analysis cell of a Quantachrome



**Figure 4.** Micropore size distribution (left) and cumulative micropore volume (right) for hydrotalcite after thermal pretreatment at 200 °C (lower curve) and 300 °C (upper curve). The mesopore structures were calculated from N<sub>2</sub> at -196 °C adsorption isotherm data using the H-K method (assuming slit-type pores).



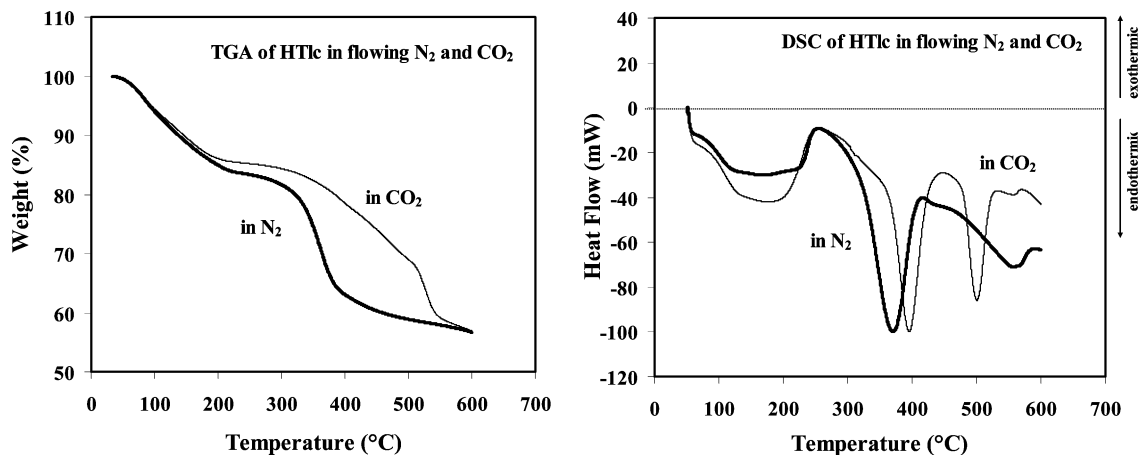
**Figure 5.** Mass spectrometer response for evolved gases upon heating of the HTlc at 20 °C/min in flowing He.

Autosorb-1-C with mass spectrometer attachment. The sample (approximately 1 g) was first used to collect adsorption isotherm data for sorption of CO<sub>2</sub> at 300 °C. The sample was then cooled to room temperature and then heated at 20 °C/min in flowing He. A plot of the mass spectrometer response to the effluent gas concentration versus temperature is shown in Figure 5. Note that there appears to be some moisture in the He carrier gas.

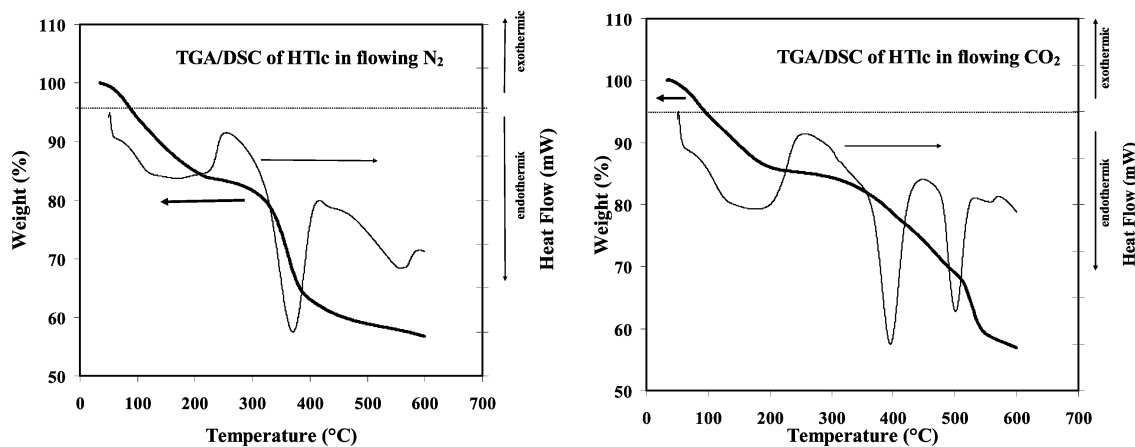
Most of the loosely held water (mass 18) in the interlayer space is lost before the material is heated to

300 °C, with the majority being evolved in the 120–180 °C range. There is some initial decarbonation starting at about 100 °C, but the CO<sub>2</sub> evolution (mass 44) does not increase significantly until the material is heated to >200 °C. The CO<sub>2</sub> evolution peaked at about 360 °C. At about that same temperature, an evolution of mass 18 begins, peaking at about 470 °C before decreasing. This is likely the result of the disappearance of OH<sup>-</sup> groups (dehydroxylation), likely in the Al-OH-Mg configuration. As the material further decomposes, there is a sharp evolution of O<sub>2</sub> (mass 32) that peaks at about 620 °C and a second peak of CO<sub>2</sub> evolution peaking at about 760 °C. These are the result of the complete decomposition of the material to a solid solution of MgO and Al<sub>2</sub>O<sub>3</sub>. Hibino et al.<sup>21</sup> observed that 20–30% of carbonates remain after heating the Mg-Al-CO<sub>3</sub> HTlc (with Al/(Al + Mg) = 0.33) to 500 °C, and they are released between 600 and 900 °C as Al<sup>3+</sup> migrates into MgO to form spinel (MgAl<sub>2</sub>O<sub>4</sub>).

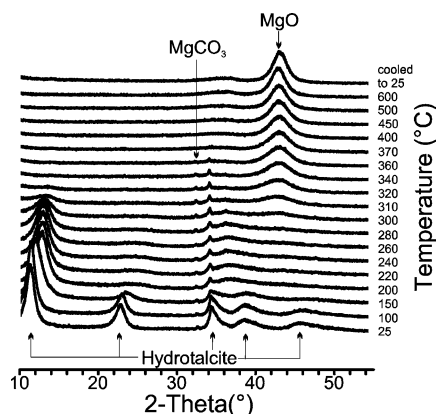
In separate experiments, approximately 10 mg of the HTlc material was placed in the TG7 sample dish. The samples were then heated at 5 °C/min in flowing N<sub>2</sub> and CO<sub>2</sub>. Separately approximately 20 mg of the material was placed in the DS7 sample holder and the samples were heated at 20 °C/min in flowing N<sub>2</sub> and CO<sub>2</sub>. The TGA profiles for the sample in N<sub>2</sub> and CO<sub>2</sub> are shown in Figure 6 (left). One can see that in both cases there is a sharp immediate decrease in weight of approximately 15% in the temperature range of 30–250 °C.



**Figure 6.** Thermogravimetric analysis of HTlc in flowing N<sub>2</sub> and CO<sub>2</sub> with a heating rate of 5 °C/min and DSC profile for HTlc in flowing N<sub>2</sub> and CO<sub>2</sub> with a heating rate of 20 °C/min.



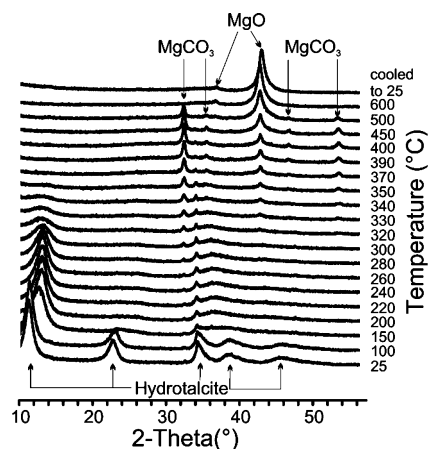
**Figure 7.** TGA/DSC scans for HTlc in flowing  $N_2$  (left) and in flowing  $CO_2$  (right). The heating rates were  $5\text{ }^\circ\text{C}/\text{min}$  for the TGA profiles and  $20\text{ }^\circ\text{C}/\text{min}$  for the DSC profiles.



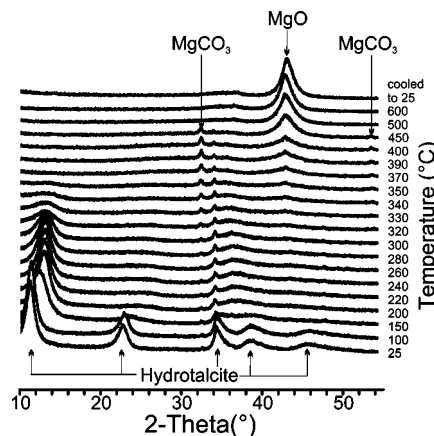
**Figure 8.** In situ HTXRD patterns for the HTlc in flowing  $N_2$  as a function of temperature.

This is almost entirely due to loss of loosely held water in the interlayer space and some initial decarbonation. The sample that was heated in flowing  $N_2$  then shows another sharp decrease in weight in the temperature range of  $300\text{--}400\text{ }^\circ\text{C}$ . This is due to a significant decarbonation through the loss of the interlayer charge compensating carbonate anion (as evolved  $CO_2$ ). The sample that was heated in flowing  $CO_2$  also shows this weight loss due to thermal decarbonation. However, the weight loss is not as abrupt due to concomitant  $CO_2$  physisorption and mineralization of the sample. There is another sharp decrease in the sample weight at about  $550\text{ }^\circ\text{C}$  that is likely due to decomposition of the mineralized  $MgCO_3$ .

Figure 6 (right) also shows the DSC scans for the material under the same conditions. The materials, under both the  $N_2$  and  $CO_2$  atmospheres, showed broad initial curves in the range of water removal (room temperature to  $250\text{ }^\circ\text{C}$ ). A large peak immediately followed, corresponding to  $CO_2$  evolution as the result of decarbonation of the interlayer charge compensating carbonate anion. The peak was at approximately  $360\text{ }^\circ\text{C}$  for the material in flowing  $N_2$  and approximately  $390\text{ }^\circ\text{C}$  for the material in flowing  $CO_2$ . For the material that was heated in flowing  $CO_2$ , there is a second exothermic peak at about  $500\text{ }^\circ\text{C}$ , which is assumed to be from  $MgCO_3$  decomposition. Both materials then show a peak at about  $550\text{--}570\text{ }^\circ\text{C}$ , which is assumed to be evolution of  $O_2$  as the structure is initially being broken down to a solid solution. For comparison, the TGA/DSC curves



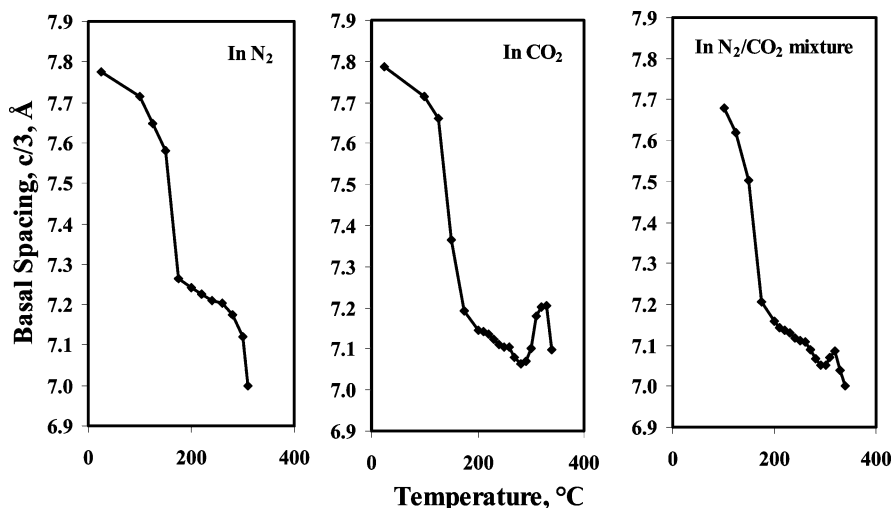
**Figure 9.** In situ HTXRD patterns for the HTlc in flowing  $CO_2$  as a function of temperature.



**Figure 10.** In situ HTXRD patterns for the HTlc in a flowing mixture of  $N_2/CO_2$  (80/20) as a function of temperature.

are shown again in Figure 7 with the curves in  $N_2$  shown on the left and in  $CO_2$  on the right.

**X-ray Diffraction.** To further characterize structural changes that may affect  $CO_2$  adsorption on HTlc, HTXRD patterns were collected under varying conditions. The diffraction patterns are shown in Figures 8 (in  $N_2$ ), 9 (in  $CO_2$ ), and 10 (in  $N_2/CO_2$  mixture). The peak shift, most readily observed with the  $d_{003}$  peak in each figure, was due to three mechanisms: the thermal expansion of the unit cell, sample displacement as the bulk sample shrank due to desorption of water, and



**Figure 11.** Basal spacing ( $d/3$ ) versus temperature from in situ XRD of HTlc in N<sub>2</sub>, CO<sub>2</sub>, and an N<sub>2</sub>/CO<sub>2</sub> (80/20) mixture.

collapse of the interlayer spacing as water desorbed. To measure the change in the interlayer spacing, the positions of the (003) and (006) peaks were determined at each temperature using a profile fitting routine. By using both diffraction peaks, the effects of sample displacement were deconvoluted from the changes in the  $c$  lattice parameter so that the  $c$  lattice parameter could be accurately calculated. The unit cell used for HTlc consisted of three basal layers stacked along the  $c$ -direction; therefore, the basal layer thickness was one-third of the  $c$  lattice parameter. The resulting plot of the basal layer thickness as it changed with temperature is shown in Figure 11. The basal spacing decreased from approximately 7.8 to 7.2 Å when the HTlc was heated from room temperature to 200 °C in any of the tested atmospheres. In N<sub>2</sub>, the basal spacing decreased to 7.1 Å when heated to 300 °C and reached a minimum spacing of 7.0 Å before the HTlc peaks became unobservable at >310 °C. When the HTlc was heated in CO<sub>2</sub> or in the N<sub>2</sub>/CO<sub>2</sub> (80/20) mix, the basal layer thickness decreased to 7.0 Å at 290 °C. The HTlc peaks persisted up to 340 °C; however, from 300 to 330 °C the basal layer actually increased from 7.0 to 7.2 Å in the CO<sub>2</sub> and 7.1 Å in the N<sub>2</sub>/CO<sub>2</sub> mix. Above 330 °C, the basal layer then decreased to 7.1 Å in CO<sub>2</sub> and 7.0 Å in the N<sub>2</sub>/CO<sub>2</sub> mix before the  $d_{003}$  peak disappeared above 340 °C. The HTlc behaved very similarly up to 300 °C in the CO<sub>2</sub> and N<sub>2</sub>/CO<sub>2</sub> mix; however, above 300 °C the basal layer “swelled” more in CO<sub>2</sub>. Assuming that the thickness of one layer of the HTlc is 4.8 Å, as has been previously reported,<sup>29</sup> then the interlayer spacing therefore decreased from 3.0 to 2.4 Å after heating from room temperature to 200 °C and then to ~2.2 Å after further heating to 300 °C. After the material is heated beyond 300–340 °C, the well-defined layered structure is lost and the material becomes nearly amorphous. The structural nature of the material upon heating to higher temperatures is dependent on the environment in which it is heated. The slight swelling of the basal spacing just before the structure collapses (for the CO<sub>2</sub> and N<sub>2</sub>/CO<sub>2</sub> samples) is likely due to adsorption of CO<sub>2</sub> in the interlayer space.

*XRD in N<sub>2</sub>.* The HTlc that was heated in the flowing N<sub>2</sub> (Figure 8) showed very small peaks at ~32° ( $2\theta$ ) that

were identified as MgCO<sub>3</sub>. These peaks were present at room temperature and disappeared by 360 °C. This indicates that there was some small amount of MgCO<sub>3</sub> initially present in the HTlc sample. In the Mg–Al–CO<sub>3</sub> HTlc structure the CO<sub>3</sub><sup>2-</sup> anion has very weak, if any, direct interaction with the Mg<sup>2+</sup> and Al<sup>3+</sup> structural cations.<sup>30</sup> A broad peak at ~43° ( $2\theta$ ), indicating the presence of MgO, becomes noticeable at 300 °C and continues to grow with heating.

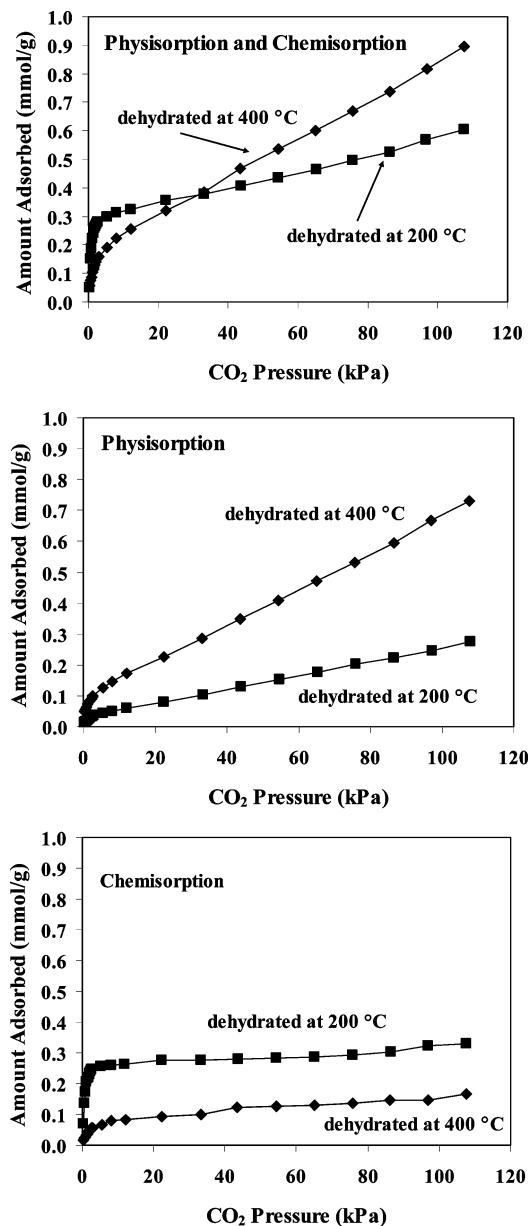
*XRD in CO<sub>2</sub>.* The diffraction patterns for the HTlc when heated in flowing CO<sub>2</sub> are shown in Figure 9. The patterns are similar to those in flowing N<sub>2</sub> in that the low-angle  $d_{003}$  peaks shift to the right with heating (as mentioned earlier). However, the MgCO<sub>3</sub> peak at 33° ( $2\theta$ ) continues to grow, indicating mineralization of the HTlc with increasing temperature in the flowing CO<sub>2</sub>. The peak then disappeared between 500 and 600 °C, indicating decomposition of the MgCO<sub>3</sub> (though in the thermal decomposition experiment described earlier, a second CO<sub>2</sub> peak, which was ascribed to MgCO<sub>3</sub> decomposition, was not seen until the sample had been heated to greater than 700 °C. As with the material that was heated in N<sub>2</sub>, a peak at ~43° ( $2\theta$ ) begins to form when heating above 300 °C. However, the MgO peaks, when compared to those of the HTlc in flowing N<sub>2</sub>, are much sharper and well defined.

*XRD in N<sub>2</sub>/CO<sub>2</sub> Mixture.* Figure 10 shows the in situ HTXRD patterns for the HTlc in a flowing mixture of N<sub>2</sub>/CO<sub>2</sub> (80/20 vol %) as a function of temperature. The diffraction patterns seem to have commonality with both the previously described conditions. The familiar MgCO<sub>3</sub> peak at 33° ( $2\theta$ ) is again seen in this sample; however, the intensity does not grow with temperature, as was obvious with the material that was heated in flowing CO<sub>2</sub>. The peak had then disappeared from the patterns collected at 500 °C, earlier than that in flowing CO<sub>2</sub>. As with the previous samples, the MgO peak at ~43° ( $2\theta$ ) begins to form when heating above 300 °C. However, these peaks seem much sharper and better defined than those of the patterns collected in flowing N<sub>2</sub>, but not as sharp and clearly defined as those collected in flowing CO<sub>2</sub>. In general, the MgO peaks are sharper in the flowing CO<sub>2</sub>, wider in the flowing N<sub>2</sub>, and between

(29) Calvini, F.; Trifiro, E.; Vaccari, A. *Catal. Today* **1991**, *11*, 173.

(30) Yang, W.; Kim, Y.; Liu, P. K. T.; Sahimi, M.; Tsotsis, T. T. *Chem. Eng. Sci.* **2002**, *57*, 2945.





**Figure 12.** Adsorption isotherms for CO<sub>2</sub> adsorption on HTlc at 200 °C after the material had been preheated in vacuo at 200 and 400 °C (as indicated on the plots). The combined isotherm (physorption + chemisorption, shown in the top plot) was measured first. The sample chamber was then evacuated under vacuum to desorb the physisorbed component and the isotherm measurement was repeated for the physorption component (shown in the middle plot). The chemisorbed portion (shown in bottom plot) was determined via difference between the initial (combined) and second (physorption) isotherms.

for the N<sub>2</sub>/CO<sub>2</sub> mixture. All of the peaks are broader than the instrumental profile, indicating that there is a sample effect that is causing the peaks to broaden. This can be caused by crystallite size, indicating that larger MgO crystallites are grown in CO<sub>2</sub> than in N<sub>2</sub> (and somewhere between for the N<sub>2</sub>/CO<sub>2</sub> mixture). This will be explored in continued studies with this hydrocalcite material.

**Adsorption of CO<sub>2</sub>.** The focus of this work was to determine how thermally induced structural changes in the HTlc affect the adsorption of CO<sub>2</sub> at high temperatures. In most of our experiments, CO<sub>2</sub> adsorption

**Table 2. Physisorption Capacities (at 200 °C and 107 kPa) Normalized to Total Surface Area and Pore Volume for HTlc after Heating to 200 and 400 °C in Vacuum**

sample	BET SA, m <sup>2</sup> /g	pore vol, cm <sup>3</sup> /g	physisorption		
			mmol/g	μmol/m <sup>2</sup>	mmol/cm <sup>3</sup>
HTlc-200	66.1	0.144	0.274	4.145	1.903
HTlc-400	183.7	0.305	0.731	3.979	2.397

isotherms are measured at temperatures between 300 and 400 °C. However, in an effort to capture structural effects, in this work adsorption isotherms were measured at 200 °C. Samples of the HTlc were first preheated in a vacuum to 200 and 400 °C. As shown earlier, there is a significant difference in the pore volume and total surface area for samples that have been heated to 200 and 400 °C. The combined (physorption plus chemisorption) isotherm was measured first and the sample was then evacuated, removing only the physically (weakly) adsorbed gas. The adsorption isotherm measurement was then repeated to obtain the physorption component. The chemisorption (strong) isotherm was then determined by the difference in the combined isotherm and the physorption (weak) isotherm. The isotherms for CO<sub>2</sub> adsorption at 200 °C are shown in Figure 12. The combined isotherms are shown in the top plot. The isotherms differ in that the material that was heated to 200 °C (HTlc-200) shows a high adsorption at low CO<sub>2</sub> pressures before stabilizing to a moderate increase in adsorption with increasing pressure. The sample that was heated to 400 °C (HTlc-400) shows less adsorption at lower CO<sub>2</sub> pressures with a less pronounced “knee” in the isotherm. The amount of CO<sub>2</sub> adsorbed then increases with increasing pressure with a capacity of ~0.9 mmol CO<sub>2</sub>/g of sorbent at 107 kPa pressure. The capacity of the HTlc-200 sample was ~0.6 mmol/g at 107 kPa pressure. To understand this we look at the physorption and chemisorption contributions.

**Physorption.** The physorption isotherms are given in Figure 12 (middle plot). Both isotherms have a similar aspect, but the HTlc-400 sample has a greater capacity. From the look of the HTlc-400 isotherm, it does appear that this is some additional chemisorption contribution. This is consistent with previous observations of an irreversible decline in the adsorption capacity with cycling.<sup>17</sup> But most of the increase in physorption capacity for the HTlc-400 sample is easily explained by the increase in total surface area and pore volume upon heating to temperatures greater than 300 °C. Table 2 shows the absolute CO<sub>2</sub> physorption capacity for both samples (HTlc-200 and HTlc-400 at 200 °C and 107 kPa) and the physorption normalized to total surface area and the total pore volume. When normalized to the total surface area and total pore volume, the physorption amount is approximately the same for both samples.

**Chemisorption.** The chemisorption isotherms are given in Figure 12 (bottom plot). The isotherms look very similar with sharp initial adsorption at low CO<sub>2</sub> pressures before reaching a saturation point, where the isotherm is nearly flat with increasing pressure. However, contrary to the physorption capacities, the sample that had been preheated to 200 °C had the greater chemisorption capacity (~0.33 mmol/g versus ~0.17 mmol/g at 200 °C and 107 kPa). The combined chemisorption and chemisorption capacities (at 200 °C



**Table 3. Adsorption Capacities (at 200 °C and 107 kPa) for HTlc after Heating to 200 and 400 °C in Vacuum**

sample	CO <sub>2</sub> adsorption capacity, mmol/g			% chemisorption contribution
	combined	physisorption	chemisorption	
HTlc-200	0.604	0.274	0.330	54.6%
HTlc-400	0.896	0.731	0.165	18.4%

and 107 kPa) for both samples are given in Table 3. The percent of the chemisorption contribution to the total capacity is also given in Table 3. More than half (54.6%) of the total CO<sub>2</sub> adsorption capacity for the HTlc-200 sample came from the chemisorption contribution, which represented less than 20% of the total capacity for the HTlc-400 sample.

**Discussion of Results.** The high-temperature adsorption of CO<sub>2</sub> on Mg–Al–CO<sub>3</sub> hydrotalcite-like compound is affected by structural changes that take place upon heating of the material. Upon heating to 200 °C, most of the loosely held water is lost but most of the CO<sub>3</sub><sup>2-</sup> is still present. The material retains its layered structure, but the interlayer spacing is collapsed due to the loss of the water, and the space is decreased by ~0.3 Å. However, there is no significant increase in total surface area or total pore volume, and physisorption of CO<sub>2</sub> at 200 °C (and lower) is limited as a result. Chemisorption of CO<sub>2</sub> at high temperatures is likely due exclusively to mineralization of the sample by the reaction of Mg and CO<sub>2</sub> to form MgCO<sub>3</sub>. This is seen in the high-temperature XRD patterns for samples in flowing CO<sub>2</sub> and in the N<sub>2</sub>/CO<sub>2</sub> mixture. The charge-compensating carbonate anion in the interlayer spacing does not interact directly with framework Mg<sup>2+</sup>. However, the sample that had been heated to 200 °C must have had increased availability of the Mg<sup>2+</sup> cation, since the chemisorption is higher than for the sample that had been heated to 400 °C and represents a higher percentage contribution to the total combined adsorption capacity. Constantino and Pinnavaia<sup>14</sup> studied the relationship between the composition and structure of various Mg–Al layered double hydroxides on catalytic activity. They found that the crystalline LDH intercalates (activated below the temperature of structural collapse) were more reactive for base-catalyzed reactions than the amorphous oxides formed by thermal decomposition of the LDH structures. Tichit et al.<sup>23</sup> reported a progressive increase in the lattice *a* parameter as with increasing temperature and progressive collapse of the layered structure. They attribute this to migration of Al<sup>2+</sup> (whose ionic radius is slightly lower than that of Mg<sup>2+</sup>) from the framework octahedral brucite-type layers to tetrahedral sites in the interlayer. Bellatto et al.<sup>22</sup> have estimated this to be 10% (at a minimum) of the Al<sup>3+</sup> at 200 °C. This effectively makes the framework

Mg<sup>2+</sup> ions more available for reaction with CO<sub>2</sub>. The Mg<sup>2+</sup> ions are then less available in samples that have been heated to above ~300 °C, where the layered structure collapses and the material becomes amorphous. Upon heating to 400 °C the CO<sub>3</sub><sup>2-</sup> in the interlayer is decomposed and the material is completely dehydrated and partly dehydroxylated. It is at this point that a three-dimensional network is formed. Bellatto et al.<sup>22</sup> suggested that the 3-D network poses constraints on the octahedral layers, which contract along the plane. An increase in surface area occurs along with the contraction of the octahedral layer. The 3-D structure consists of a close-packed oxygen network, which traps in its interstices a disordered cation configuration with octahedral (M<sup>2+</sup>) and tetrahedral (M<sup>3+</sup>) cations. The increased surface area and pore volume and the decreased availability of the Mg<sup>2+</sup> cation favor physisorption over chemisorption for these samples.

The hydrotalcite-like compounds are very open to physical and chemical manipulation. There are numerous combinations of M<sup>3+</sup> and M<sup>2+</sup> cations and interlayer charge-compensating anions that can be used to create HTlcs with unique properties. The structure and properties of the materials are affected by the thermal history as well. With the proper understanding of these structure–property relationships, HTlc may conceivably be synthesized and tailored for use in a CO<sub>2</sub> separation and capture technology, such as pressure swing adsorption (PSA).

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